

# Development of PID Controller for Controlling Desired Level of Coupled Tank System

H.I Jaafar, S.Y.S Hussien, N.A Selamat, M.S.M Aras, M.Z.A Rashid

**Abstract**—The industrial application of Coupled Tank System (CTS) are widely used especially in chemical process industries. The overall process need liquids to be pumped, stored in the tank and pumped again to another tank for certain desired level. Nevertheless, the level of liquid in tank need to be controlled and flow between two tanks must be regulated. This paper presents development of Proportional-Integral-Derivative (PID) controller for controlling the desired liquid level of the CTS. Various conventional techniques of PID tuning method will be tested in order to obtain the PID controller parameters. Simulation is conducted within MATLAB environment to verify the performances of the system in terms of Rise Time ( $T_r$ ), Settling Time ( $T_s$ ), Steady State Error (SSE) and Overshoot (OS). Four techniques which are trial and error method, auto-tuning method, Ziegler-Nichols (Z-N) method and Cohen-Coon (C-C) method will be implemented and all the performance results will be analyzed. It has been demonstrated that performances of CTS can be improved with appropriate technique of PID tuning methods.

**Index Terms**— Coupled Tank System (CTS), PID Controller, PID Tuning Method, Water Level Control.

## I. INTRODUCTION

Real time control involves algorithms to control a certain processes. In order to study the performance in terms of implementation in real time and each control features, control of level of a Coupled Tank System (CTS) is chosen. This application is widely used in the process industries especially in chemical industries [1]. It is often essential that the liquid to be supplied in tanks. It will be stored up in tanks and transferred it to the other tank as per requirement. The liquid must be maintained at a specific height or in a certain level. If the level cannot be maintained at the specific height as requirement, it can bring losses to the company or industries.

A common control problem in process industries is to control the fluids level in storage tanks and chemical blending. The flow of the liquid into and out the tank must be regulated as to achieve a constant desired liquid level as fluid to be supplied at a constant rate. This process are performing in closed loop condition because open loop is not practical and identification process more complicated especially in industrial production processes [2-3]. Closed loop process is very important due to safety or production restriction reasons [4].

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**H.I. Jaafar**, Faculty of Electrical Engineering (FKE), Universiti Teknikal Malaysia Melaka (UTeM), Hang Tuah Jaya, 76100 Durian Tunggal, Malaysia.

**S.Y.S. Hussein**, Faculty of Electrical Engineering (FKE), Universiti Teknikal Malaysia Melaka (UTeM).

**N.A. Selamat**, Faculty of Electrical Engineering (FKE), Universiti Teknikal Malaysia Melaka (UTeM).

**M.S.M. Aras**, Faculty of Electrical Engineering (FKE), Universiti Teknikal Malaysia Melaka (UTeM).

**M.Z.A. Rashid**, Faculty of Electrical Engineering (FKE), Universiti Teknikal Malaysia Melaka (UTeM).

The Coupled Tank CTS-001 is a computer controlled CTS that is used for liquid level control as shown in Figure 1.



Figure 1: Coupled Tank CTS-001

The concept of virtual instrumentation is introduced in CTS-001. The need for traditional dedicated user interfaces on individual instrumentations can be eliminated by using virtual instrumentation techniques [5]. Besides, the computer can be used as the tool of communications between the hardware and software. Through the software analysis, it enables to carry out the function of oscillation and display the input and output response. From the system, it also can verify the parameter of the model which can be derived from the mathematical modeling [6-10]. This output response from the modeling function can be taken as the benchmark to achieve good response after implemented it in the CTS. The performance can be easily monitored in MATLAB simulation.

## II. PID CONTROLLER

The industrial, CTS are widely used in consumer liquid processing and chemical processing industry. In order to control the level of the liquid, a conventional PID controller had been implemented. PID Controller is the most controllers that always been used in industrial control because of easy and simple to implement [11-15]. There are several methods to obtain the parameters for PID controllers such as trial and error method, Ziegler-Nichols (Z-N) method and Cohen-Coon (C-C) method. Tuning method is very important in control system. The values of the parameters in the controller can affect the performance of the system. The performance of the system can be generally improved by proper tuning but it also can be worsen the performance with poor tuning. In PID, there are several tuning method that can be used to find the desired control response.

### A. Trial and Error

Trial and Error is one of the method and easiest way to obtain the value of PID parameter. In this method, no mathematical is required. However, the optimal value of the parameter is not guaranteed. The value of  $K_I$  and  $K_D$  need to be set first as zero before increasing the  $K_P$ . This will takes a lot of time and experience skill to obtain the best result.

**B. Ziegler-Nichols (Z-N)**

Z-N is the tuning method that is widely used of tuning PID controller. It is developed by John G. Ziegler and Nanthaniel B. Nichols in 1940s [16]. In this tuning method,  $K_I$  and  $K_D$  gain are also need to be set first to zero. Then  $K_P$  is increased until it reaches the ultimate gain,  $K_U$  at which the output of the loop starts to oscillate in the oscillation period,  $T_U$ .

**C. Cohen-Coon (C-C)**

C-C tuning method is the second popular after the Z-N tuning method. The method was published by Cohen and Coon in 1953 [17]. This method is more flexible than Z-N tuning method in the wider variety of processes. Z-N method work well only on the processes where the dead time is less than half the length of the time response compared to the C-C method where the dead time is less than two times the length of the time constant.

**III. MATHEMATICAL MODELING OF CTS**

It is vital to understand the mathematics modeling of the behavior of Coupled Tank System (CTS). In this system, the nonlinear dynamic model is observed and the linearization process is done from the nonlinear model.

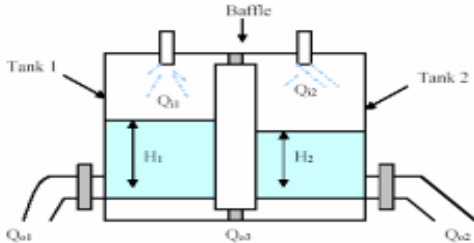


Figure 2: Schematic diagram of CTS

Based on Figure 2,  $H_1$  and  $H_2$  are the fluid level in Tank 1 and Tank 2. It is measured with respect to the corresponding outlet. Considering a simple mass balance, the rate of change of fluid volume in each tank equals the net flow of fluid into the tank. Therefore, the equation for Tank 1 and Tank 2 are:

$$A_1 \frac{dH_1}{dt} = Q_{i1} - Q_{o1} - Q_3 \tag{1}$$

$$A_2 \frac{dH_2}{dt} = Q_{i2} - Q_{o2} + Q_3 \tag{2}$$

where:

- $H_1, H_2$  = height of fluid in tank 1 and 2 respectively
  - $A_1, A_2$  = cross-sectional area of tank 1 and 2 respectively
  - $Q_3$  = flow rate of fluid between tanks
  - $Q_{i1}, Q_{i2}$  = pump flow rate into tank 1 and 2 respectively
  - $Q_{o1}, Q_{o2}$  = flow rate of fluid out of tank 1 and 2 respectively
- Each outlet drain can be modeled as a simple orifice. Bernoulli's equation for steady, non-viscous, incompressible shows that the outlet flow in each tank is proportional to the square root of the head of water in the tank. Similarly, the flow between the tanks is proportional to the square root of the head differential. Thus:

$$Q_{o1} = \alpha_1 \sqrt{H_1} \tag{3}$$

$$Q_{o2} = \alpha_2 \sqrt{H_2} \tag{4}$$

$$Q_3 = \alpha_3 \sqrt{H_1 - H_2} \tag{5}$$

where  $\alpha_1, \alpha_2$  and  $\alpha_3$  are proportionality constants which is depend on the coefficients of discharge, the cross sectional area of each orifice and the gravitational constant. By substitute (3), (4) and (5) into (1) and (2), the nonlinear state equations which describe the system dynamics of the CTS apparatus are:

$$A_1 \frac{dH_1}{dt} = Q_{i1} - \alpha_1 \sqrt{H_1} - \alpha_3 \sqrt{H_1 - H_2} \tag{6}$$

$$A_2 \frac{dH_2}{dt} = Q_{i2} - \alpha_2 \sqrt{H_2} + \alpha_3 \sqrt{H_1 - H_2} \tag{7}$$

In the second order configuration,  $h_2$  is the process variable and  $q_1$  is the manipulated variable and assume that  $q_2$  is zero.

The block diagram of the second-order system can be simplified as shown in Figure 3.

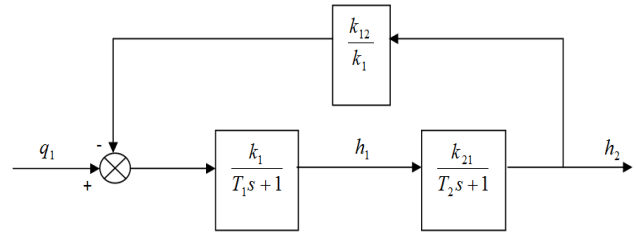


Figure 3: Block diagram of second order system

Thus, the nonlinear CTS can be obtained as:

$$\begin{aligned} \frac{h_2(s)}{q_1(s)} &= \frac{k_1 k_2}{(T_1 s + 1)(T_2 s + 1) - k_{12} k_{21}} \\ &= \frac{k_1 k_2}{T_1 T_2 s^2 + (T_1 + T_2)s + (1 - k_{12} k_{21})} \end{aligned} \tag{8}$$

where:

$$T_1 = \frac{A_1}{\left(\frac{\alpha_1}{2\sqrt{H_1}}\right) + \left(\frac{\alpha_3}{2\sqrt{H_1 - H_2}}\right)} \tag{9}$$

$$T_2 = \frac{A_2}{\left(\frac{\alpha_2}{2\sqrt{H_2}}\right) + \left(\frac{\alpha_3}{2\sqrt{H_1 - H_2}}\right)} \tag{10}$$

$$k_1 = \frac{1}{\left(\frac{\alpha_1}{2\sqrt{H_1}}\right) + \left(\frac{\alpha_3}{2\sqrt{H_1 - H_2}}\right)} \tag{11}$$

$$k_2 = \frac{1}{\left(\frac{\alpha_2}{2\sqrt{H_2}}\right) + \left(\frac{\alpha_3}{2\sqrt{H_1 - H_2}}\right)} \tag{12}$$

$$k_{12} = \frac{\frac{\alpha_3}{2\sqrt{H_1 - H_2}}}{\left(\frac{\alpha_1}{2\sqrt{H_1}}\right) + \left(\frac{\alpha_3}{2\sqrt{H_1 - H_2}}\right)} \tag{13}$$

$$k_{21} = \frac{\frac{\alpha_3}{2\sqrt{H_1 - H_2}}}{\left(\frac{\alpha_2}{2\sqrt{H_2}}\right) + \left(\frac{\alpha_3}{2\sqrt{H_1 - H_2}}\right)} \tag{14}$$

The transfer function for the plant can be obtained by substituting the parameter which was provided from the [5]. The provided parameters are shown in Table 1.

Table 1: Parameter of CTS

Parameters	Value	Unit
H <sub>1</sub>	17	cm
H <sub>2</sub>	15	cm
α <sub>1</sub>	10.78	cm <sup>3</sup> /2/sec
α <sub>2</sub>	11.03	cm <sup>3</sup> /2/sec
α <sub>3</sub>	11.03	cm <sup>3</sup> /2/sec
A <sub>1</sub>	32	cm <sup>2</sup>
A <sub>2</sub>	32	cm <sup>2</sup>

Then, all the parameters in Table 1 have been inserted into (8). Thus, the actual transfer function of the plant with the completed value is:

$$G_p(s) = \frac{h_2(s)}{q_1(s)} = \frac{0.0361}{36.9406s^2 + 12.1565s + 0.4514} \quad (15)$$

#### IV. RESULT AND DISCUSSION

The plant of the CTS is obtained from the mathematical modeling in previous section. The input voltage injected in the system is 1 Volt (V) and the level converter will convert the input voltage to the water level. For this case the desired level is 1 cm. The block diagram and the response of the system are shown in Figure 4.

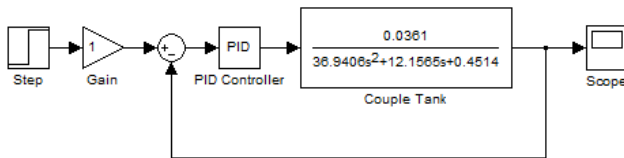


Figure 4: Control structure with PID Controller

The stability of the system can be determined by Routh-Hurwitz stability criterion as in Table 2. It is a mathematical test that is a necessary and sufficient condition for the stability of a linear time invariant (LTI) control system. Table 2 shows the Routh-Hurwitz table for the transfer functions of the CTS as in (16) based on the characteristic equation.

$$6.94s^2 + 12.16s + 0.4514 + 0.0361K = 0 \quad (16)$$

The system is determined as a stable system only if the coefficients in the first columns are all positives.

Table 2: Routh-Hurwitz table for CTS

s <sup>2</sup>	36.91	0.4514 + 0.0361K	0
s <sup>1</sup>	12.16	0	0
s <sup>0</sup>	$\begin{aligned} & \begin{vmatrix} 36.94 & 0.4514+0.0361K \\ 12.16 & 0 \end{vmatrix} \\ & \frac{12.16}{12.16} \\ & = \frac{[0 - 12.16(0.4514 + 0.0361K)]}{12.16} \\ & = 0.4514 + 0.0361K \end{aligned}$	0	0

According to Table 2, CTS is stable because it can be proved that the coefficients in the first column are all positives sign.

$$\begin{array}{l|l} s^2 & + 36.91 \\ s^1 & + 36.91 \\ s^0 & + [0.4514+0.0361K] \end{array}$$

Table 3 shows the parameters of the PID controller (K<sub>P</sub>, K<sub>I</sub> and K<sub>D</sub>). According to this table, the tuning method of PID controller has shown the capability of the system by using either calculation approach or experiences approach.

Table 3: Parameter of PID Controller

Method	Parameter		
	K <sub>P</sub>	K <sub>I</sub>	K <sub>D</sub>
Trial and error	15.00	1.00	8.00
Auto-tuning	53.40	1.54	-2.98
Ziegler-Nichols	168.00	35.00	201.60
Cohen-Coon	235.88	33.92	203.21

Table 4 shows the summary of the transient response specification of the PID controller by the classical tuning method respect to the parameters of the controller.

Table 4: Performance of CTS

Method	T <sub>s</sub> (sec)	T <sub>r</sub> (sec)	OS (%)	SSE (cm)
Trial and error	84.40	24.00	6.86	0.00
Auto-tuning	53.30	9.14	1.81	0.00
Ziegler-Nichols	32.10	3.29	38.50	0.00
Cohen-Coon	23.59	2.81	33.70	0.00

One of the transient response specifications which are settling time shows that C-C method had the fastest time for the system to reach the stable condition in the system. From the tuning method of Z-N, the response of the system is the second fastest after the C-C, compared to the other tuning method. Besides, C-C method shows that it has the fastest time in the rise time in the system followed by Z-N, auto-tuning and Trial and Error method. However, C-C method has the fastest time response for the system, but the percentage of the overshoot is higher compared to the others methods. Figure 5, 6, 7 and 8 are the performance for each method respectively.

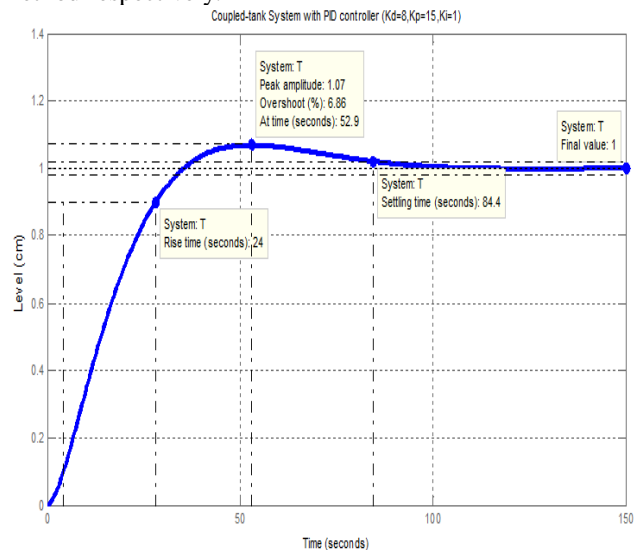


Figure 5: Performance response using Trial and Error method

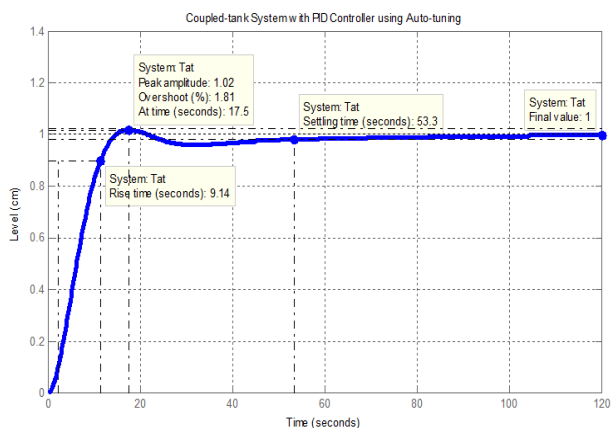


Figure 6: Performance response using Auto-Tuning method

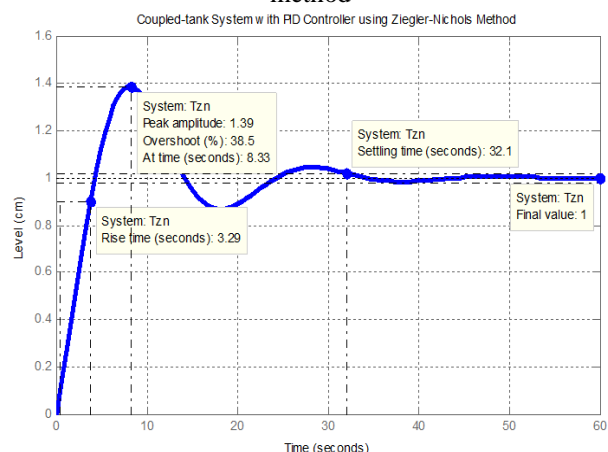


Figure 7: Performance response using Z-N method

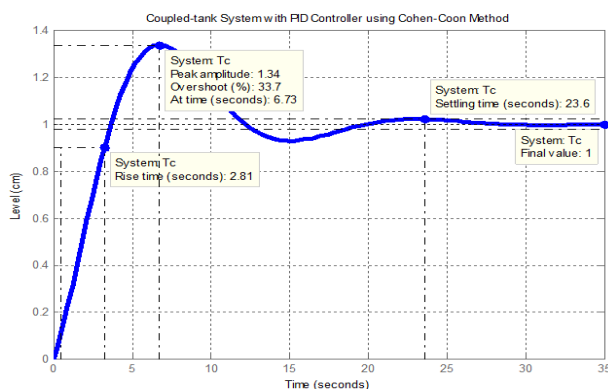


Figure 8: Performance response using C-C method

In addition, Figure 9 summarizes all the results in graphical representation.

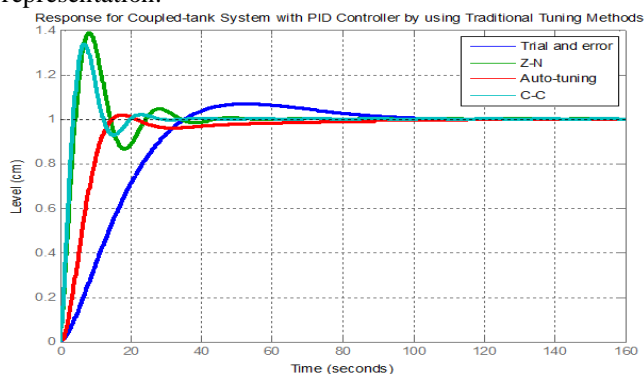


Figure 9: Response of CTS with various tuning method of PID controller

It can be concluded that by using the conventional tuning method for PID controller have their own advantages and disadvantages. For the trial and error method, it takes long time to achieve a good performance unless having enough experience to tune it. Then, it can save time. For the Z-N tuning method, it is the popular method in the industry. This method required short time to complete and easy to use than the other methods. Even though it is a popular method but through this method, it produced an aggressive gain and overshoot in the system. This method is similar to the C-C method. The process reaction curve is obtained first from the open-loop system before substituting the value in the standard recommended equation. The difference between Z-N method and C-C method is the parameters of  $T_i$  and  $T_d$  can be obtained in open-loop and closed-loop system for Z-N method but for C-C method, the parameters can only be obtained in open-loop system. Last but not least, for the Auto-Tuning method, even though it is the simplest method but the value obtained from this method does not refer on the respective parameter. The value which is obtained from this method is the combination of the parameters in PID controller.

## V. CONCLUSION

In order to control the level of the liquid, a conventional PID controller had been implemented. The parameter of the PID controller can be tuned by the traditional method such as trial and error, Z-N, C-C and auto-tuning. The performance of the system may achieve the good performance but quite difficult for finding the parameters. It required a lot of effort and experiences to obtain a good gain of the controllers. Therefore, optimization approach will be implemented to find the optimal parameters of the controller. By using this approach, a good gain and better performance is expected.

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and underactuated nonlinear system. He is an associate member of Universal Association of Computer and Electronics Engineers (UACEE).



**Hazriq Izzuan Jaafar** received his B.Eng degree in Electrical Engineering from Universiti Teknologi Malaysia (UTM), in 2008. He received the M.Eng degree in Mechatronics and Automatic Control engineering also from UTM, in 2013. Currently, he is a Lecturer at Universiti Teknikal Malaysia Melaka (UTeM) and his interests are in control system and optimization

techniques.



**Sharifah Yulsinda Syed Hussien** received her Diploma in Electrical Engineering from Universiti Teknikal Malaysia Melaka (UTeM), in 2011. Currently, she pursues her degree in Electrical Engineering in Control, Instrumentation and Automation System, UTeM.



**Nurasmiza Selamat** received his B.Eng degree in Electrical Engineering from Universiti Teknologi Malaysia (UTM), in 2009. She received the M.Eng degree in Mechatronics and Automatic Control engineering also from UTM, in 2013. Currently, she is a Lecturer at Universiti Teknikal Malaysia Melaka (UTeM) and her interests are in control system and optimization techniques.



**Mohd Shahrieel Mohd Aras** is a lecturer at Faculty of Electrical Engineering, Universiti Teknikal Malaysia Melaka UTeM. He currently pursues his PhD in Control and Automation, Faculty of Electrical Engineering, Universiti Teknologi Malaysia. His current research is focusing on control system design of underwater technology. His primary interests related to nonlinear underwater robotics and Artificial Intelligence.



**Mohd Zamzuri Ab. Rashid** received his B.Eng degree in Mechatronics from International Islamic University in 2005. He finished his MSc. in Mechatronics from International Islamic University in 2012. Currently, he serves as lecturer in Universiti Teknikal Malaysia Melaka. His current research interests include unmanned system