

# Kinetic of 4-Chlorophenols Biodegradation by Arthrobacter chlorophenolicus A6

Naresh Kumar Sahoo

**Abstract:** Chlorophenols are listed as priority pollutants both by European community and US EPA. Biodegradation of p-chlorophenol (4-CP) was investigated in batch shake flasks by *Arthrobacter chlorophenolicus A6* at initial 4-CP concentrations between 25 to 350 mg l<sup>-1</sup>. The rate of 4-CP removal decreased with increasing initial 4-CP concentrations due to toxic effects on the microorganisms. The growth and biodegradation kinetic of the culture was evaluated. The batch growth profile of the *A chlorophenolicus A6* followed substrate inhibition kinetics with the estimated biokinetic parameters of  $K_{si} = 272 \text{ mg l}^{-1}$ ,  $K_s = 65 \text{ mg l}^{-1}$  for 4-CP respectively. High inhibition constant ( $K_{SI} = 272 \text{ mg l}^{-1}$ ) with a  $K_{SI}/K_s$  ratio of 4.18 indicates superior 4-CP biodegradation potential of the *A chlorophenolicus A6*. The maximum rate of 4-CP degradation has been achieved at an optimum substrate concentration of  $S_{max} = (K_S K_{SI})^{1/2} / (65 \times 272)^{1/2} = 133 \text{ mg l}^{-1}$ .

**Keywords:** Biodegradation, *Arthrobacter chlorophenolicus A6*, 4-Chlorophenol, Substrate inhibition kinetics.

## I. INTRODUCTION

The major industries associated with chlorophenol are such as petrochemical, pharmaceutical, wood preserving, integrated iron and steel plant, pesticide and paper [1,2,3]. Further during the disinfection of drinking water and bleaching of pulp in paper industry significant amount of chlorinated phenol are produces. Therefore, effluent from these above mentioned industries causes a severe human health hazards as well serious damage to the environment. Chlorophenol is one of the hazardous waste and placed in 166th position out of the 1467 number of the national priority pollutant list as per US EPA. Chronic exposure of chlorophenol from polluted environment is suspected to be carcinogen and is highly embryo toxic in nature [4,5]. Similarly also exhort toxicity to aquatic organisms [6]. Wild et al, [7] reported the concentration of primary pollutants present in 12 sewage sludge's such as; 19.6–86.3 g/L of 2,4-dichlorophenol. However maximum allowed chlorophenol concentration is 10 µg/L in drinking water [8]. The above mentioned chlorophenol concentration in the industrial effluent and sewage sludge are beyond the permissible limit, so there is a urgent need to enhance the rate and concentration of chlorophenols removal from wastewater. There are several methods available in treatment of phenolic wastewater for instance; volatilization, adsorption, photocatalytic degradation, electrochemical methods, and solvent extraction [9]. However, poor efficiency, generation of toxic by product and high cost, are the major drawback of these removal strategies. The eco friendly biodegradation method is an attractive alternative to the above mentioned

traditional methods. There are several reports available in literature on biodegradation of chlorophenols by mixed culture and pure culture bacterial species such as *Flavobacterium* sp., *Pseudomonas* sp., *Sphingomonas* sp., *Mycobacterium* sp., *Flavobacterium* sp., *Rhodococcus* sp., *Streptomyces* sp., *Arthrobacter* sp., etc are the most potential species. Among the various species, actinomycetes can secret both, extracellular as well as intracellular enzymes thus this species is able to degrade chlorophenols efficiently. Furthermore, the active cleft of the enzymes are altered mainly at leu80, Asp83, Val107 aminoacids positions, which facilitates its broad specificity nature in degradation of wide different type of pollutants present in real industrial wastewater and can interact with wide different toxic substrates occur in actual industrial wastewater, along with chlorophenols [10]. It is highly essential to enhance the rate and concentration of chlorophenol biodegradation.

In order to design and optimize the operational conditions for treatment of contaminated wastewater using bioreactor system, knowledge on pollutant biodegradation kinetics and microbial growth profile is playing the vital role. However, biomass growth and 4-chlorophenol degradation kinetic using actinomycetes strain is very scanty. Although actinomycetes are the proved to be the most efficient species in chlorophenol biodegradation however, only limited reports are available on biodegradation of the chlorophenol by actinomycetes species. The present investigation demonstrates the growth and 4-CP degradation kinetics of *A chlorophenolicus A6*, at diffrent initial concentration of chlorophenol have been evaluated.

## II. MATERIALS METHODS

### A. Chemicals and Reagents

Analytical grade 4-CP was procured from Sigma Aldrich (Germany). All other chemicals and reagents used in the study were procured from Merck (India), HiMedia, (Mumbai, India).

### B. Preparation of Inoculums

The biodegradation of 4-CP was carried out by employing a minimum salts medium (MSM) (g l<sup>-1</sup>: K<sub>2</sub>HPO<sub>4</sub> 2.6, NH<sub>4</sub>NO<sub>3</sub> 0.58, KH<sub>2</sub>PO<sub>4</sub> 0.4, MgSO<sub>4</sub> 0.17, FeCl<sub>3</sub> 0.002 and CaCl<sub>2</sub> 0.038) and pH 7.4, with 300 mg l<sup>-1</sup> 4-CP [11]. The seed culture cells were grown in the above mentioned MSM with 0.3% yeast extract in an incubator shaker for 40 h at 30 °C and 210 rpm. Then the cells centrifuged (8000 g

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at 10 °C) and were washed in sterile phosphate buffer (PBS, pH 7.5). Then the microbial cells were adapted to 4-CP by growing overnight with MSM containing 300 mg l<sup>-1</sup> of 4-CP as the only carbon source. After this adaptation period the cells were centrifuged (8000g, 15 min at 10°C), washed in 1X PBS (pH 7.5) and were then employed as the inoculums for the degradation of 4-CP . The initial biomass concentration in the inoculums was 0.1 OD600nm.

#### C. Growth and degradation kinetic of 4-CP

Shake flask experiments were carried out by using Erlenmeyer flasks (250 mL) were charged with 100 mL of optimised mineral salt media as mentioned earlier. Different amounts of 4-CP were added to the separately to each flasks to yield 4-CP concentrations at a level of 25, 50, 100, 200, 250, 300, 350 mg l<sup>-1</sup> respectively. Rest of the experimental procedure were similar to as above.

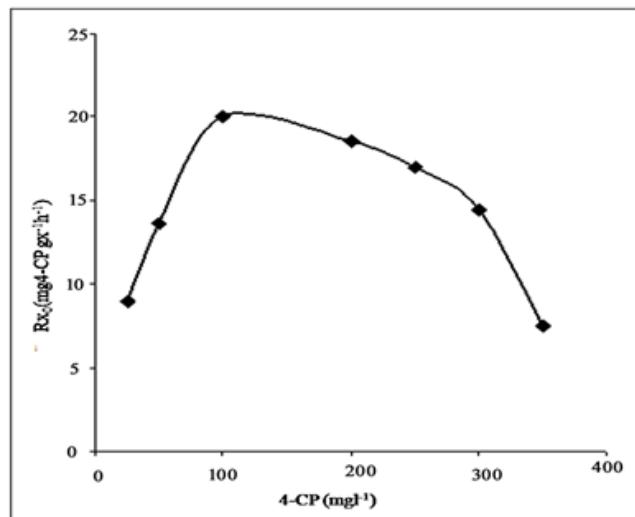
#### D. Analytical Methods

Estimation of biomass concentration was performed by measuring its optical density (OD600nm) in a UV-visible spectrophotometer (Perkin Elmer U.S.A, Model lambda-45). 4-CP concentration of 4-CP from the collected samples were measured by reverse phase HPLC system employing an Onsphere C-18 column (Varian Prostar 210). Detection of 4-CP was carried out using a UV detector at wavelength of 280 nm. The mobile phase used in the estimation of 4-CP was a mixture of acetonitrile-water (80:20, v/v). The experiment was carried out at a flow rate of 0.8 ml/min and at 28°C and the retention time of 4-CP was observed at 5.6 min.

### III. RESULTS AND DISCUSSION

#### A. Growth and degradation kinetic of 4-CP

Figure 1 demonstrates variation of 4-CP degradation rates with initial concentration of 4-CP. It is observed from the Figure 1 that, the rate of 4-CP degradation increases with increase in initial 4-CP concentration up to 100 mg l<sup>-1</sup>, On the other hand, rate of 4-CP decreases when the initial 4-CP concentration increases beyond 100 mg l<sup>-1</sup>. This observation clearly reveals substrate inhibitory effects of 4-CP on the microbial cell at concentrations more than 100 mg l<sup>-1</sup>. In this conditions the degradation rate of 4-CP declines from 20 to 8 mg l<sup>-1</sup> h<sup>-1</sup> when initial concentration of 4-CP raises from 140 to 350 mg l<sup>-1</sup>. Since the actinomycetes strain follows a typical substrate inhibition kinetics patterns as shown in Figure 1, a literature existing non-competitive substrate inhibition kinetics model was applied to estimate the biokinetic parameters associated with degradation of 4-CP by the *A chlorophenolicus A6* as follows [12].



**Figure1. Variation of 4-CP specific degradation rate with change in initial concentration.**

$$R_{s0} = \frac{kX_0S_0}{K_S + S_0} \frac{K_{SI}}{K_{SI} + S_0} = \frac{kX_0}{(1+K_S/S_0)(1+S_0/K_{SI})} \quad 1$$

$$R_{x0} = \frac{R_{s0}}{X_0} = \frac{kS_0}{K_S + S_0} \frac{K_{SI}}{K_{SI} + S_0} \quad 2$$

Where,  $S_0$  stands for the initial concentration of 4-CP (mg l<sup>-1</sup>),  $X_0$  represents the initial biomass concentration of the actinomycetes culture (mg l<sup>-1</sup>),  $R_{s0}$  is denotes for 4-CP degradation rate (mg 4-CP l<sup>-1</sup> h<sup>-1</sup>),  $K_S$  represents the half saturation constant (mg l<sup>-1</sup>),  $k$  stands for the rate of biodegradation constant (h<sup>-1</sup>) and  $K_{SI}$  represents the inhibition constant on microbial cell due to 4-CP (mg l<sup>-1</sup>).  $R_{s0}$  is determined by using the initial concentration versus time and the slope gives the rate (mg l<sup>-1</sup> h<sup>-1</sup>). The specific rate of 4-CP degradation ( $R_{x0}$ ) can be calculated as  $R_{s0}/X_0$  where  $X_0$  is 0.014 g l<sup>-1</sup>. The first term in equation (1) correspond to Monod rate expression for the rate of 4-CP biodegradation by the actinomycetes species. Whereas, the second term of the equation (1) indicates the non-competitive substrate inhibition pattern of 4-CP on the microbial cells. When the initial concentrations of 4-CP is low (4-CP < 100 mg l<sup>-1</sup>), at this condition the inhibition term can be ignored ( $S_0 \gg K_{SI}$ ) therefore the Equation 1 can be renovated as follows .

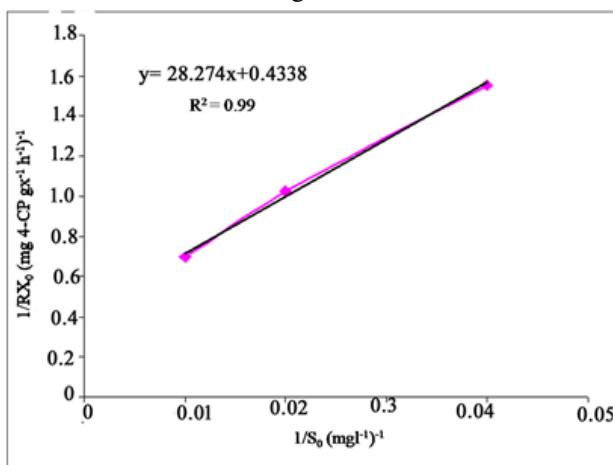
$$R_{s0} = \frac{kX_0S_0}{K_S + S_0} = \frac{R_{m0}S_0}{K_S + S_0} \quad 3$$

$$R_{x0} = \frac{R_{s0}}{X_0} = \frac{kS_0}{K_S + S_0} \quad 4$$

Where,  $R_{m0} = kX_0$  represents the maximum rate of 4-CP biodegradation (mg 4-CP l<sup>-1</sup> h<sup>-1</sup>). At a initial concentration of 4-CP lower than 100 mg l<sup>-1</sup>, the equation 3 can be expressed in double reciprocal form as follows.

$$\frac{1}{R_{x0}} = \frac{1}{k} + \frac{K_S}{k} \frac{1}{S_0} \quad 5$$

From Equation 5 the slope of plot between  $1/R_{x0}$  versus  $1/S_0$  represents value of  $K_S/k$  where as the value of  $1/k$  can be calculated from the intercept of the straight line. Figure 2 demonstrates the plot between  $1/R_{x0}$  versus  $1/S_0$  at 4-CP concentration less than  $100 \text{ mg l}^{-1}$ .



**Figure 2 Double reciprocal plot of  $1/R_{x0}$  versus  $1/S_0$  at 4-CP concentration less than  $100 \text{ mg l}^{-1}$ .**

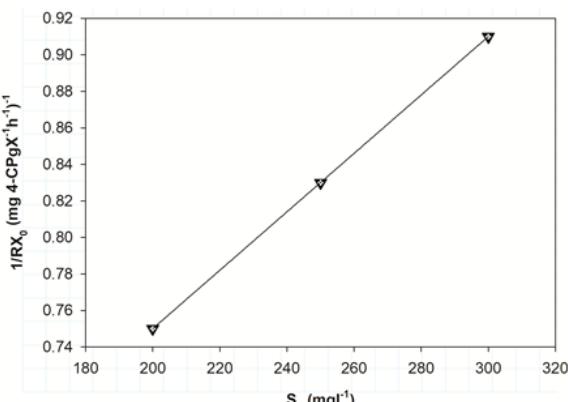
From the slope and intercept of the best-fit line with very high determination coefficient value ( $R^2 = 0.99$ ) the following values were found. The 4-CP biodegradation rate constant ( $k$ ) was calculated to  $2.3 \text{ mg 4-CP g}^{-1} \text{ h}^{-1}$  from the intercept of the best-fit line. Similarly half saturation constant ( $K_S$ ) was estimated to be  $65.17 \text{ mg l}^{-1}$ . When the concentration of 4-CP beyond  $100 \text{ mg l}^{-1}$  the first term of equation (1) can be ignored ( $S \gg K_S$ ) and the substrate inhibition term becomes the rate determining factor. Therefore, when the concentration of 4-CP is more than  $100 \text{ mg l}^{-1}$ , rate equation can be expressed as follows.

$$R_{S0} = kX_0 \frac{K_{SI}}{K_{SI} + S_0} \quad 6$$

$$\frac{1}{R_{x0}} = \frac{R_{S0}}{X_0} = \frac{kK_{SI}}{K_{SI} + S_0} \quad 7$$

The linear form of the Equation 6 can be expressed as follows:

$$\frac{1}{R_{x0}} = \frac{1}{k} + \frac{S_0}{kK_{SI}} \quad 8$$



**Figure 3. Double reciprocal plot between  $1/R_{x0}$  versus initial 4-CP ( $S_0$ ) concentration at higher range.**

Figure 3 represents the plot between  $1/R_{x0}$  versus  $S_0$  at 4-CP concentration more than  $100 \text{ mg l}^{-1}$ . However, 4-CP

concentration  $350 \text{ mg l}^{-1}$  was not included in the model as the biodegradation rate since was very less and not fitting for this model in this experiment. The slope of the best fitted line with high determination coefficient ( $R^2 = 0.99$ ) represents  $(1/(kK_{SI}))$  and the intercept of the best fitted line correspond to the rate constant ( $1/k$ ). The 4-CP biodegradation rate constant ( $k$ ) was calculated to  $2.3 \text{ mg 4-CP g}^{-1} \text{ h}^{-1}$  from the intercept of the best-fit line. Similarly inhibition constant ( $K_{SI}$ ) was calculated to be  $271.7 \text{ mg l}^{-1}$ .

An effort has been made to compare the kinetics parameters estimated in the present study with that of the literature reported values. The magnitude of half saturation constant ( $K_S$ ) indicates the degree of affinity of 4-CP to the cells of *A. chloropehnolicus A6* its growth. The estimated  $K_S$  value ( $65 \text{ mg l}^{-1}$ ) is lower than with that of the literature reported values in the range of  $75.7$ -  $92.4 \text{ mg l}^{-1}$  for biodegradation of phenolic compounds by pure and mixed cultures system [13-15]. The lower value of half saturation constant obtained in the study ( $65 \text{ mg l}^{-1}$ ) indicates the higher affinity of 4-CP to the cells of the microorganism for its growth. A lower half saturation constant indicates that, 4-CP is more readily degraded utilized by the *A. chloropehnolicus A6*. In the present investigation, the higher specific degradation rate of  $2.3 \text{ mg 4-CP g}^{-1} \text{ h}^{-1}$  acquired might be due to the *A. chloropehnolicus A6* biomass shunting quite a smaller amount of the electrons for the restoration of NADPH, which is typically used for activation of the monooxygenase enzyme system involved with biodegradation of phenolic compounds compared to other bacterial system. However, further investigation is necessary to authenticate this feature. The magnitude of kinetic parameter  $K_{SI}$  indicates the degrees of toxicity tolerance of the cells of the microorganisms to the concentration of 4-CP. Larger the  $K_{SI}$  value indicates toxicity tolerance of microorganism to substrate is very high. In general for degradation of phenolic compounds by different microbial system the reported  $K_{SI}$  values in the range of  $37.75$  to  $400 \text{ mg l}^{-1}$  [15, 16, 17, 18]. The larger  $K_{SI}$  value ( $272 \text{ mg l}^{-1}$ ) obtained in the present study reveals 4-CP toxicity tolerance of the *A. chloropehnolicus A6* is found to be very high. The maximum rate of 4-CP degradation is estimated by applying the following kinetics model at an optimum substrate concentration of  $S_{max} = (K_S K_{SI})^{1/2} = (65 \times 272)^{1/2} = 133 \text{ mg l}^{-1}$ .

#### IV. CONCLUSIONS

The present study revealed that *Achlorophenolicus A6* could be employed for treatment of wastewater contaminated with 4-CP efficiently within a short period of time and at a very high concentration i.e.  $350 \text{ mg l}^{-1}$ . The rate of 4-CP degradation decreases with rise initial 4-CP concentrations due to toxic effects of 4CP exerted on microbial cell at its higher initial concentration. The experimental results of substrate inhibition kinetic values are better fitted with Pamukoglu and Kargi model. High inhibition constant ( $K_{SI} = 273 \text{ mg l}^{-1}$ ) with a  $K_{SI}/K_S$  ratio of 4.18 indicates superior 4-CP biodegradation potential of the

A chlorophenolicus A6. Biokinetic parameters obtained in the study for degradation 4-CP were close agreement with that of literature reported values. The biokinetic parameters obtained in the study will invariably useful in design and operating of bioreactor system for treatment of industrial wastewater contaminated with phenolic pollutants.

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