

# Experimental and Numerical Analysis of Composite Wick Heat Pipes using Ethanol

Purbasha Bhadra, B. Ch. Nookaraju

**ABSTRACT:** Warmth pipes come convenient now-a-days as they work with most noteworthy warmth conductance contrasted with some other method of warmth move and accessible over wide scope parameters. In the present investigation de-ionized water stream in plain thermo siphon, Sintered Copper wick and Helical scored heat pipes with synchronous vanishing, adiabatic and buildup wonder are contemplated utilizing Heat pipe test gear. In this hardware warmth pipe exposed to foreordain heat load an obstruction radiator at its evaporator end water coat with controlled progression water is utilized disperse warmth vitality at condenser end. Every one temperatures are estimated necessary computations are done get rate efficiencies at different stream rates warmth inputs. The exhibition warmth funnels correlation between their efficiencies is done. The sintered copper wick structure pipe have been found capable when stood out from other two with heat inputs beginning from 50 to 800 watts evaporator 30, condenser 72, adiabatic 110, flate heat pipe width 7.6mm, thickness 3.4 mm, first dia 6mm warmth pipe holder thickness in 0.5mm working liquid ethanol wick in view prevailing Capillarity property. The varieties of evaporator and condenser surface temperatures are plotted for changing warmth information sources and stream rate changes at condenser water coat. ANSYS programming is utilized for computational investigation and exploratory outcomes are in great concurrence with the examination.

## I. INTRODUCTION

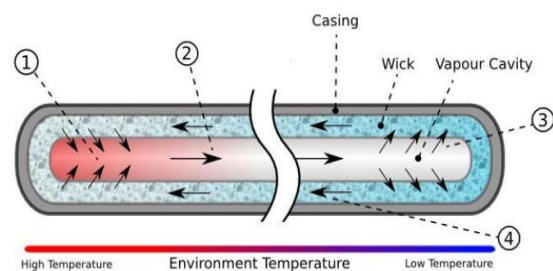
The innovation warming and cooling frameworks is one most essential zones Mechanical building. Any place steam is utilized, any place hot or cold liquids are required we will discover heat exchanger. They are used to warmth cool homes, work environments, markets, strip malls, automobiles, trucks, trailers, aero-planes, and other transportation systems. They are used to process sustenance, paper, oil, and in various other present day systems. They are found superconductors, combination control labs, shuttles, and propelled PC frameworks. The rundown applications, in both low and cutting edge ventures, is for all intents and purposes unending. In our fundamental investigation thermodynamics heat move, we examined structure control volume vitality equalization and its application too many building issues, including to essential warmth exchanger issue. In this module, we will stretch out warmth exchanger examination to incorporate convection rate condition, show philosophy for anticipating heat exchanger execution that incorporate both plan execution rating issues. In event that genuine structure streams, heat burden, and temperatures can't be accomplished in testing, test information must extrapolated (considering tube stopping) to process general warmth move coefficient and contrast it with the plan esteem.

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Be that as it may, any estimation should likewise think about vulnerability mistake in trial estimations warmth and stream. Moreover, even before general coefficient is registered, test information must surveyed have adequate precision. This might be done pretest where test parameters are assessed, made decision about whether general warmth move coefficient can definitively found. For control plant faculty such investigation is trying because way that data must drawn from instrument structure activity, heat move applications, factual hypothesis. Surely lot of distributed work as of now manages these points. Albeit factual strategies are various, numerous systems are cumber few hard apply real power plant heat exchangers as estimations from working units are regularly restricted test size quality plant staff must have generally basic handy, however successful, technique pass judgment on information. Be that may, rearranged approach explicit to control plant coolers isn't promptly accessible in regular writing. Information on instrument sensor exactness, effect of number sensors, information testing interims, sensible factual certainty level are portion elements to considered, particularly on account temperature estimation. To address this, present work, drawing from industry models, exhibits brought together, down to earth factual methodology and evaluates these variables so heat exchanger temperature information might be effectively and immediately surveyed. Besides, test estimations are displayed to encourage utilization proposed strategy. Despite the fact that focus is on temperature estimation, strategy can effectively reached out to stream estimation or some other parameter



## 1.2 Performance Parameters of Heat Pipe

Heat pipe has three components.

1. Casing
2. Working fluid
3. Wick structure

## 1.3 Composite Wick Heat Pipe

Composite wick structures use advantages of having little pores for making high narrow siphoning and having gigantic pores for broadening porousness fluid return way. Anew, most direct kind of composite wick is screen wick, close to that two screens with various pore sizes are utilized.



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Two or three wraps screen with noteworthy pore measure is utilized against inward channel divider for fluid return way, singular wrap screen with broadly littler pore assess is put contacting fume space to grow high narrow weight. Essentially, hub forests moored by single wrap little pore screen can manage colossal amounts issues related with homogeneous center score wick. Since screen adequately isolates fluid and fume streams, entrainment fluid into fume stream by interfacial shear is about cleared out. Correspondingly, this composite wick can utilized in antagonistic gravity fields since screen makes required limited weight.

## II. LITERATURE REVIEW

- **Hong Seok ,Seongpilet al., 2018,**“ altering slim weight and bubbling system of small scale permeable wicks finished with graphe oxide". He acquainted exceptionally permeable wicking surface with advance slim driven stream in heat pipe. Miniaturized scale permeable copper covered with graphite oxide (GO) expanded basic warmth motion, narrow weight wicking impact. Little pores GO builds slim weight because hydrophilic nature of GO covering, contact edge among fluid and surface as diminished. Over top GO covering decreases permeability which reduces pool-boiling performance.

- **Yong tanget al., 2017** investigated some tests to increase thermal presentation ultra thin heat pipe. The tests are chemical deposition, sintering, composition surface after deposition capillary rise experiments. Test outcomes show that slim power kept wick structures was bigger typical wick.

- **Yanping Huanget al., 2017** "Exploratory investigation of warmth move start-up circle heat pipe multi scale permeable wicks". He considered the impact warmth move and start up circle heat pipe with multi scale permeable wicks and contrasted and ordinary monoporous wicks, composite multiscale permeable wicks abbreviated beginning up time, diminished divider temperature, stifled temperature unsteadiness LHP. A cooperative energy between warm conductivity protection was accomplished, which guaranteed high warm conductivity for essential layer wick decent warm protection for whole wick. This extraordinarily decreased warmth spillage from evaporator to pay chamber.

- **Kumaresanet al., 2014** considered and thought about warmth move execution attributes of sintered wick and work wick heat pipes utilizing CuO/DI water Nano liquids at different warmth information and tendency edges. It is discovered that warmth transport limit sintered wick heat pipe is 14.3% more contrasted and work wick heat pipe under equivalent working conditions. Essentially, higher decrease in surface temperature 27.08% is watched for sintered wick heat pipe with 1.0wt% CuO/DI water Nano liquids contrasted and work wick heat pipe. The tendency point and weight level CuO nanoparticles altogether impact warmth presentation both warmth pipes. Ideal tilt points of 45° and 60° separately are watched for sintered wick and work wick heat pipes, though ideal weight rate is equivalent (1 wt.%) for both cases. At these ideal conditions, decrease in warm opposition of 49.64% and 35.44% and an improvement in warm conductivity of 36.50% and 29.84% are separately watched for both sintered wick and work wick heat pipes. At last it is presumed that warm exhibition of

sintered wick heat pipe is superior to anything that of work wick heat pipe.

- **M.K Russellet al., 2011** concentrated impact of direction on exhibition of U shape heat pipe parameters for example heat info and directions. Warm obstruction of sintered wick heat pipe was seen as steady over its working extent for all directions. In furrowed wick heat pipe warm obstruction in upset U direction had fundamentally higher warm opposition.

## III. SCOPE AND OBJECTIVES

### 3.1 Motivation to the Present Work

As electronic devices get smaller, architects and engineers are looked with developing test staying aware need to improve processing speed inside shrinking form factor. Speedier processors require expanded power utilization, which creates heat and smaller form factors require more noteworthy scaling down implementation used to scatter that heat. These contemplations are driving shrewd architects and engineers to think as far systemic solutions in which each thought in devices power condition is inspected for most noteworthy improvement. As rule, prerequisites power condition request that heat dissemination must be relative to power dispersal given device. Power dissemination is measure of power squandered by device (i.e., power dissipation is reliant on capacitance logic components, operating voltage swing, and operating frequency). Despite fact that processors in mobile phones, for instance, regularly utilize only couple of hundred milliwatts of power, quite bit this is essentially lost to heat.

Customary strategies for cooling electronic hardware incorporate enhancing outline of printed circuit board, Using thermal interface materials to fill tiny air holes and utilizing of fans .These techniques are supplanted by coordination of heat pipes channels which gives productive cooling

### 3.2 Methodology:

- Mass flow rate fluid in condenser section water was used and now also used 0.01 kg/sec but in future will continue with 0.02, 0.03 kg/sec.
- Heat input given in evaporator section and eight levels were used 50,100,150,200,250,300,350,400 watts.
- Tilt angle heat pipe now were used 15° but in future will continue with more four levels 30°,45°,60°,90°

## IV. EXPERIMENTAL INVESTIGATIONS



Fig 4.1 Experimental setup of a heat pipe



#### 4.1 Experimental Setup:

The equipment is very versatile and can be used for checking performances of different heat pipes for by varying different parameters like heat input and flow rate with reference to different angle inclination. Experimental setup consists following components

- 1.Evaporator 2. Condenser 3. Control unit 4.Thermocouple
- 5.Water sink/tank 6. Measuring jars and stop watch:

#### 4.2 Experimental results:

S.NO	Qin(W)	Te(°C)	Tc(°C)	Tout(°C)	Tin(°C)	Rth(°C/W)	h(W/sq.m °C)	Π=(Qout/Qin)*100
1	50	44.4	30.7	28.8	28.9	0.274	366	30
2	100	55.5	32.1	29.6	29.5	0.234	429	49
3	150	69.9	32.4	30.3	29.9	0.25	400	46
4	200	86.7	32.8	30.6	30.4	0.2715	369	39
5	250	52.6	30.9	28.8	28.9	0.086	1154	57
6	300	62.9	32.3	30.2	29.7	0.102	982	78
7	350	62.5	35.8	35.8	35.7	0.0762	1313	80
8	400	75.9	36.1	36.0	35.9	0.0995	1007	95

Table-5 observation for At 15° angle and m-0.02 kg/sec

S.NO	Qin(W)	Te(°C)	Tc(°C)	Tout(°C)	Tin(°C)	Rth(°C/W)	h(W/sq.m °C)	Π=(Qout/Qin)*100
1	50	31.1	30.8	26.5	26.1	0.045	4837	33.48
2	100	32.0	30.6	26.9	26.5	0.041	5823	25.02
3	150	33.2	31.2	27	26.7	0.040	6540	27.86
4	200	34.9	31	27.5	27.2	0.0396	6116	25.08
5	250	36	31.7	27.6	27.3	0.0392	5199	23.40
6	300	38.6	32.9	28.5	27.8	0.0398	4512	19.50
7	350	42.9	32.5	29.5	28.7	0.0399	3711	28.66
8	400	45.2	32.9	30.5	29.8	0.040	3000	20.9

Table-7 observation for At 60° angle and m-0.02 kg/sec

S.NO	Qin(W)	Te(°C)	Tc(°C)	Tout(°C)	Tin(°C)	Rth(°C/W)	h(W/sq.m °C)	Π=(Qout/Qin)*100
1	50	32.1	27.9	28.4	28	0.044	2200	50.12
2	100	34.6	33.8	29.5	28.9	0.039	2700	41.5
3	150	35.5	34.9	30.3	29.4	0.030	3342	33.44
4	200	37.7	35.5	31.5	30.4	0.025	3828	3.44
5	250	39.5	37.8	31.6	30.8	0.024	4042	30
6	300	42.4	39.2	32	31.2	0.035	3500	27.86
7	350	46.5	42.2	32.5	31.4	0.045	2800	33.44
8	400	50.1	46.7	34.7	32.9	0.043	2050	37.62

Table-8 observation for At 90° angle and m-0.02 kg/sec

S.NO	Qin(W)	Te(°C)	Tc(°C)	Tout(°C)	Tin(°C)	Rth(°C/W)	h(W/sq.m °C)	Π=(Qout/Qin)*100
1	50	31.8	29.5	28	26.9	0.045	2000	33.42
2	100	33.6	29.5	28.9	27.8	0.039	2400	24.09
3	150	36	30	29.3	28.9	0.040	2790	27.86
4	200	39.8	31.7	29.7	29.1	0.0382	3100	25.09
5	250	41.9	31.9	31.0	29.5	0.0393	3260	55.09
6	300	44.3	32	31.8	31.2	0.0398	2600	22.29
7	350	45.9	32.1	32.8	31.9	0.0399	2148	22.49
8	400	48.6	32.2	32.3	32.1	0.040	2000	20.09

Table-9 observation for At 15° angle and m-0.03 kg/sec

S.NO	Qin(W)	Te(°C)	Tc(°C)	Tout(°C)	Tin(°C)	Rth(°C/W)	h(W/sq.m °C)	Π=(Qout/Qin)*100
1	50	32	31.2	29.4	29	0.026		50.18
2	100	33.5	31.9	29.6	29.3	0.016		50.17
3	150	34.3	32.8	30.2	29.7	0.009		50.17
4	200	35.4	32.7	30.6	29.9	0.015		43.90
5	250	36.9	32.7	30.9	30	0.018		40.15
6	300	39.4	33.6	31.7	30.8	0.019		37.20
7	350	42.3	33.7	31.9	30.9	0.023		46.60
8	400	46.8	35.4	32	31.6	0.029		18.80

Table-10 observation for At 30° angle and m-0.03 kg/sec

S.NO	Qin(W)	Te(°C)	Tc(°C)	Tout(°C)	Tin(°C)	Rth(°C/W)	h(W/sq.m °C)	Π=(Qout/Qin)*100
1	50	33.8	31.7	29.2	29	0.038	3000	50.15
2	100	34.8	31.8	29.6	29.5	0.031	3500	38.60
3	150	36	32.3	29.9	29.3	0.025	4200	41.9
4	200	39.3	33.2	30.6	30	0.023	4600	43.82
5	250	42.8	33.7	30.8	30	0.021	4830	40.12
6	300	45.5	34	31.9	30.9	0.030	3900	41.10
7	350	47.2	34.1	32.3	31.1	0.031	3200	39.40
8	400	49.6	34.5	32.4	31.2	0.036	2800	34.49

Table-11 observation for At 60° angle and m-0.03 kg/sec

S.NO	Qin(W)	Te(°C)	Tc(°C)	Tout(°C)	Tin(°C)	Rth(°C/W)	h(W/sq.m °C)	Π=(Qout/Qin)*100
1	50	32.6	30.4	29.8	29.5	0.040	2700	75.25
2	100	35	31	30.3	29.7	0.037	3000	62.7
3	150	35.8	31.5	30.8	30.5	0.029	3418	75.25
4	200	37.4	32.2	31	30.3	0.025	3973	43.90
5	250	38	32.9	31.4	30.1	0.024	4108	40.15
6	300	41.7	32.9	32.2	31.4	0.033	3200	38.60
7	350	46.5	32.3	32.5	31.6	0.039	2800	35.80
8	400	47.8	32.3	32.6	31.5	0.038	2500	35.5

Table-12 observation for At 90° angle and m-0.03 kg/sec

S.NO	Qin(W)	Te(°C)	Tc(°C)	Tout(°C)	Tin(°C)	Rth(°C/W)	h(W/sq.m °C)	Π=(Qout/Qin)*100
1	50	32	29.9	29.7	29.5	0.041	2200	75.25
2	100	34.7	30.5	29.9	29.6	0.040	2500	50.14
3	150	36.4	30.7	30.4	29.9	0.038	2900	59.50
4	200	38.9	30.8	30.8	29.8	0.036	3200	58.52
5	250	40.2	31.5	31.7	30.4	0.034	3349	62.6
6	300	44	31.9	32.5	30.8	0.0396	2850	60.18
7	350	46.1	31.6	32.6	30.7	0.0398	2350	75.25
8	400	47.9	31.6	32.7	30.6	0.040	2050	71.65

#### 4.3 CFD Analysis

CFD strategies comprise numerical arrangements of mass, Momentum and vitality preservation with different conditions like species transport. Two fundamental stages involve arrangement of CFD issues. In the first place, entire liquid field partitions to little components their names are work, afterward halfway differential conditions clarify transport marvels in liquid stream are utilized for these components.



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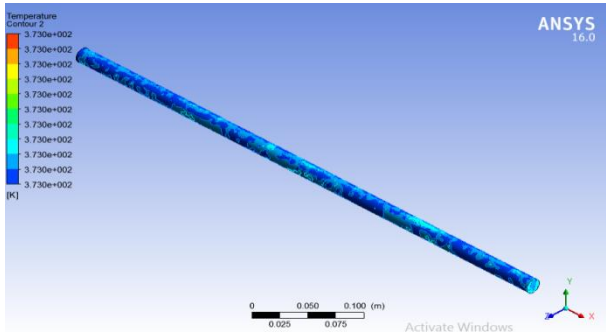
Thus, numerous non-straight conditions show up which need to understand at same time. The arrangement of these conditions achieve with numerical calculation techniques. Protection conditions for compressible stream

## 4.4 Materials Of Heat Pipes:

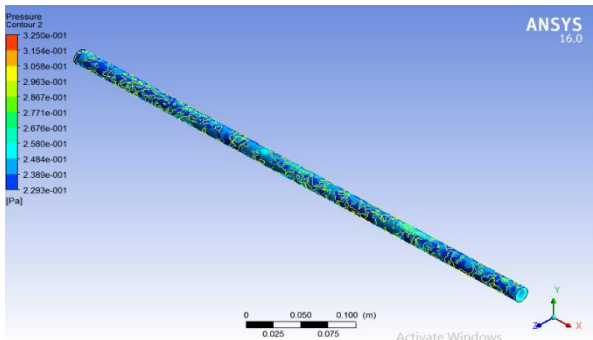
- Working fluid : Ethanol
- Container material : Copper
- Type of wick : Composite wick (sintered powder and screen mesh of 250 mesh number)
- Properties of Ethanol : Melting point at (-112°C)  
Boiling point at ATM pressure(78°C)

Useful range (0 to 130°C)

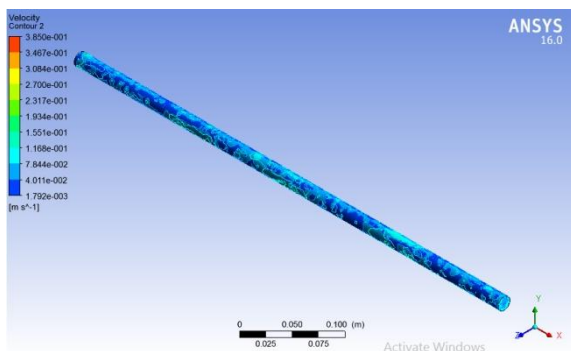
Temperature:



Pressure:



Velocity:



## V. CONCLUSION:

In this examination impact of warmth pipe process parameters for example mass stream rate ( $\dot{m}$ ) of coolant, tendency point ( $\theta$ ) and heat input control ( $Q$ ) on warm execution of the helical notched warmth pipe were contemplated tentatively.

1. Heat exchange coefficient increments with increment of warmth input, increment of mass stream rate and tilt of point. With increment heat input heat move coefficient increments up to certain point since more water

is disintegrated so warmth can be expelled adequately by stage changes further increment warmth input it diminishes on account quicker fume delivers progressively interfacial obstruction between stream fume and condensate and will bring about lacking come back to condensate to evaporator area.

2. With the utilizing tilt edge, presentation of warmth pipe is diminishing

3. As mass stream pace of water builds, exhibition warmth pipe likewise expanding.

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